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 $\frac{\partial \left(\rho Y_{k}\right)}{\partial t}$

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$$\frac{\partial \rho}{\partial t} + \frac{\partial \left(\rho \, u_{\rm i}\right)}{\partial x_{\rm i}} = 0. \tag{2.1}$$

In the context of reactive flows a formulation of the conservation of mass for *n* species is desirable. In this case a species source term or sink terminal likely to be present due to the reaction. In contrast to the total mass relative a diffusion term has to be included here, since species from the mass be patially non-uniform. Defining the mass fraction of the species from term.

$$Y_{\rm k} = \frac{\rho_{\rm k}}{\sum\limits_{k}^{n} \rho_{\rm k}},\tag{2.2}$$

$$\frac{\partial \left(u_{j}Y_{k} \right)}{\partial x_{i}} = \frac{\partial}{\partial x_{i}} \left[\rho D \frac{M_{k}}{d} \frac{\partial X_{k}}{\partial x} - Y_{k}V_{i}^{c} + \mathcal{S}_{i}, \right]$$
(2.3)

where the first term on the right hand side a counts for diffusion, with X_k being the molar fraction of species k, V_k the nullar weight of species k and D_k being the diffusion coefficient for species k. The term V_i^c is defined as

$$V_{\rm i}^{\rm c} = \sum_{k=1}^{n} D_k \frac{M_{\rm k}}{M} \frac{\partial X_{\rm k}}{\partial x_{\rm i}}$$
(2.4)

and ensures global mass conservation after introduction of the diffusion law [2].

2.1.2 The Compressible Navier-Stokes Equations

The Navier-Stokes equations are nameline in and physician Claude Louis Marie Henri matician and physician Sir George Ga can be derived from a balance of model in the mathematical structure in the mathematical structu

2.1.1 The Conservation of Mass

The conservation of mass can be derived by considering the mass-fluxes entering and leaving an infinitely small volume element. In the absence of a source of mass, the equation of the conservation of mass can be written as follows:

$$\frac{\partial \rho}{\partial t} + \frac{\partial \left(\rho \, u_{\rm i}\right)}{\partial x_{\rm i}} = 0. \tag{2.1}$$

In the context of reactive flows a formulation of the conservation of mass for n species is desirable. In this case a species source term or sink term \mathscr{S}_k is likely to be present due to the reaction. In contrast to the total mass balance, a diffusion term has to be included here, since species fractions may be spatially non-uniform. Defining the mass fraction of the species k:

$$Y_{k} = \frac{\rho_{k}}{\sum\limits_{i=1}^{n} \rho_{k}},$$
(2.2)

$$\frac{\partial \left(\rho Y_{k}\right)}{\partial t} + \frac{\partial \left(\rho u_{j} Y_{k}\right)}{\partial x_{j}} = \frac{\partial}{\partial x_{j}} \left[\rho D_{k} \frac{M_{k}}{M} \frac{\partial X_{k}}{\partial x_{j}} - Y_{k} V_{i}^{c}\right] + \mathscr{S}_{i}, \qquad (2.3)$$

where the first term on the right hand side accounts for diffusion, with X_k being the molar fraction of species k, M_k the molar weight of species k and D_k being the diffusion coefficient for species k. The term V_i^c is defined as

$$V_{i}^{c} = \sum_{k=1}^{n} D_{k} \frac{M_{k}}{M} \frac{\partial X_{k}}{\partial x_{i}}$$
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